

IN THE SPECIFICATION:

The specification as amended below with replacement paragraphs shows added text with underlining and deleted text with ~~strike through~~.

(1) Please amend the paragraph beginning at page 3, line 9 as follows:

--Polyphenylene ethers not only have excellent mechanical properties, excellent electrical properties (such as dielectric constant and dielectric dissipation factor) and excellent heat resistance, but also have excellent dimensional stability. Therefore, polyphenylene ethers have been used in a wide variety of fields. However, the moldability of a polyphenylene ether is poor. For improving the moldability of a polyphenylene ether, Examined Japanese Patent Publication No. Sho 45-997 discloses a technique in which a polyamide is added to a polyphenylene ether, to thereby obtain a polyamide-polyphenylene ether alloy. Further various new techniques relating to polyamide-polyether alloys are proposed in, for example, U.S. patent Nos. ~~431508~~ 4,315,086, 4,732,938 and 4,659,760. Nowadays, polyamide-polyether alloys are used in a very wide variety of fields, such as exterior parts for automobiles.--

(2) Please amend the paragraph beginning at page 12, line 3 as follows:

--6. The shaped resin article according to item 1 above, wherein the polyamide (A) comprises at least one polyamide component having a terminal amino group content of from 1×10^5 10^{-5} mol/g to 4×10^5 10^{-5} mol/g.--

(3) Please amend the paragraph beginning at page 23, line 10 as follows:

--Further, it is preferred that polyamide (A) used in the shaped resin article of the present invention comprises at least one polyamide having a terminal amino group content of from 1×10^5 10^{-5} to 4×10^5 10^{-5} ~~mol/kg~~ mol/g, more advantageously from 2×10^5 10^{-5} to

3×10^5 ~~10^{-5} mol/kg mol/g~~. In such a case, there is no particular limitation with respect to the terminal carboxyl group content; however, it is preferred that the terminal carboxyl group content is at least 5×10^5 10^{-5} mol/g or more, more advantageously from 6×10^5 10^{-5} to 13×10^5 10^{-5} ~~mol/kg mol/g~~.--

(4) Please amend the paragraph beginning at page 51, line 14 as follows:

--Examples of compatibility agents which can be used in the production of the shaped resin article of the present invention include those which are described in detail in Unexamined Japanese Patent Laid-Open Specification Nos. Hei 8-~~8869~~ 8-48869 (corresponding to EP 204,416 685,527) and Hei 9-124926 (corresponding to EP 747,439). All of the conventional compatibility agents described in these patent documents can be used in the present invention, and the compatibility agents can be used individually or in combination.--

(5) Please amend the paragraph beginning at page 66, line 17 as follows:

--In the present invention, the amount of the additional component(s) incorporated into the shaped resin article is not more than 100 parts by weight, relative to 100 parts by weight of the total weight of polyamide (A), polyphenylene ether (B), partially hydrogenated block copolymer ~~(A)~~ (C) and the compatibility agent.--

(6) Please amend the paragraph beginning at page 69, line 13 to page 71, line 3 as follows:

--As an apparatus used for producing the resin composition, there can be mentioned a twin-screw extruder having a first inlet and at least one second inlet which are provided, respectively, at upstream and downstream portions of the extruder, wherein the first inlet is provided with a screw-type gravimetric feeder and a belt-type gravimetric feeder,

and the second inlet is provided with another screw-type gravimetric feeder. Using such a twin screw extruder, the production of the resin composition can be performed by any of the following methods (1) to (3): (1) a method in which a mixture of a block copolymer and a polyphenylene ether is fed to the extruder from the first inlet by the belt-type gravimetric feeder, and a compatibility agent is fed to the extruder through the first inlet by the screw-type gravimetric feeder, thereby melt-kneading together the above-mentioned mixture and the compatibility agent at the upstream portion of the extruder, while feeding a polyamide to the extruder from the second inlet, thereby melt-kneading the resultant mixture at the downstream portion of the extruder; (2) a method in which a polyphenylene ether is fed to the extruder from the first inlet by the belt-type gravimetric feeder, and a mixture of a compatibility agent and a block copolymer is fed to the extruder from the first inlet by the screw-type gravimetric feeder, thereby melt-kneading together the polyphenylene ether and the above-mentioned mixture, while feeding a polyamide to the extruder from the second inlet, thereby melt-kneading the resultant mixture at the downstream portion of the extruder; and (3) a method in which a mixture of a polyphenylene ether in the form of a powder and a block copolymer is fed to the extruder from the first inlet by the belt-type gravimetric feeder, and a compatibility agent and a polyphenylene ether in the form of pellets are fed to the extruder from the first inlet by the screw-type gravimetric feeder, thereby melt-kneading together the polyphenylene ether, the block copolymer and the compatibility agent, while feeding a polyamide to the extruder from the second inlet, thereby melt-kneading the resultant mixture at the downstream portion of the extruder.--

(7) Please amend the paragraph beginning at page 77, line 6 as follows:

--The thus obtained polyamide had a hexamethylene isophthalamide monomer unit content of about 19 mol%, a terminal amino group content of 3.9×10^5 10^{-5} mol/g and a terminal carboxyl group content of 10.2×10^5 10^{-5} mol/g ~~per kg of the polyamide~~--

(8) Please amend the paragraph beginning at page 79, line 7 to page 80, line 25 as follows:

--Specifically, using the above-mentioned extruder, the production of pellets of a resin composition was performed as follows. First, raw materials for the resin composition were fed to the above-mentioned extruder as follows. A polyphenylene ether powder (hereinafter, referred to as "PPE1") having a reduced viscosity of 0.52 dl/g (as measured with respect to a chloroform solution thereof having a polyphenylene ether concentration of 0.5 g/dl at 30 °C) was fed to the extruder through one of the screw type gravimetric feeders (hereinafter, referred to as "feeder 1") provided at the upstream inlet of the extruder. Maleic anhydride (in the form of tablets each having a diameter of 4 to 5 mm) (manufactured and sold by Mitsubishi Chemical Corporation, Japan) (hereinafter, abbreviated to "MAH") as a compatibilizer was fed to the extruder through the other screw type gravimetric feeder (hereinafter, referred to as "feeder 2") provided at the upstream inlet of the extruder. 4 Parts by weight of a polystyrene/polyethylene butylene/polystyrene block copolymer (styrene content: 33 %)(hereinafter, referred to as "SEBS1") having a number average molecular weight (Mn) of 246,000 and 8 parts by weight of a polystyrene/polyethylene butylene/polystyrene block copolymer (styrene content: 29 %)(hereinafter, referred to as "SEBS2") having a number average molecular weight (Mn) of 98,500 were dry blended using a Henschel mixer. The resultant mixture was fed to the extruder through the belt type gravimetric feeder (hereinafter, referred to as "feeder 3") provided at the upstream inlet of the extruder. By using a tumbler, a polyamide blend was prepared by dry blending 40 parts by weight of polyamide 6,6 (hereinafter, referred to as "PA66-a") having a viscosity number of 120 ml/g, a terminal amino group content of 2.5×10^{-5} mol/g and a terminal carboxyl group content of 11.6×10^{-5} mol/g, with 10 parts by weight of polyamide 6,6 (hereinafter, referred to as "PA66-b") having a viscosity number of 130 ml/g, a terminal

amino group content of 4.2×10^5 10^{-5} mol/g and a terminal carboxyl group content of 9.1×10^5 10^{-5} mol/g. The obtained polyamide blend was fed to the extruder through the screw type gravimetric feeder (hereinafter, referred to as "feeder 4") provided at the 1st downstream inlet of the extruder.--

(9) Please amend the paragraph beginning at page 90, line 1 as follows:

--Specifically, with respect to the raw materials used in Examples 2 to 4 and Comparative Example 1, the raw materials which are different from those used in Example 1 are as follows:

Polyphenylene ether powder (hereinafter, referred to as "PPE2") having a reduced viscosity of 0.42 dl/g;

MPPE produced in Production Example 1;

Polyamide 6,6 (hereinafter, referred to as "PA66-c") having a viscosity number of 230 ml/g, a terminal amino group content of 2.4×10^5 10^{-5} mol/g and a terminal carboxyl group content of 4.8×10^5 10^{-5} mol/g; and

PA66/6I produced in Production Example 2.--

(10) Please amend the Table 1 at pages 91 to 92 as follows:

Table 1

Upstream inlet	Ex. 1	Ex. 2	Ex. 3	Ex. 4	Comp. Ex. 1
Feeder 1					
PPE-1 (parts by weight)	*1	38	38	30	38
PPE-2 (parts by weight)	*2		38		
Feeder 2					
MPPE (parts by weight)	*3			8	
MAH (parts by weight)	*4	0.2	0.3	0.3	0.3
Feeder 3					
SEBS1 (parts by weight)	*5	4	4	4	4
SEBS2 (parts by weight)	*6	8	8	8	8
1st downstream inlet					
Feeder 4					
PA66-a (parts by weight)	*7	40	40	40	
PA66-b (parts by weight)	*8	10		10	
PA66-c (parts by weight)	*9		10		50
PA66/6I (parts by weight)	*10		10		
Polyamide area ratio	%	84	94	90	67
PPE having a molecular weight of 5,000 or less	%	4.78	-	7.18	3.67
PPE having a molecular weight of 200,000 or less	%	1.45	-	0.82	3.4
PPE having a molecular weight of 200,000 or less/ PPE having a molecular weight of 50,000 5,000 or less	-	0.30	-	0.11	0.93
Coating adhesion strength (number of square coating sections left on the surface of a shaped resin article out of 100 square coating sections)		95	100	60	100
Sharpness of an image reflected in the coated surface	-	A	A	A	A
Matteness of the coated surface	-	III	II	III	I

- *1) PPE powder having a reduced viscosity of 0.52 dl/g
- *2) PPE powder having a reduced viscosity of 0.42 dl/g
- *3) MAH-modified PPE obtained by melt kneading PPE having a reduced viscosity of 0.42 dl/g with MAH
- *4) Maleic anhydride (in the form of tablets)
- *5) SEBS block copolymer (styrene content: 33 %; Mn: 246,000)
- *6) SEBS block copolymer (styrene content: 29 %; Mn: 98,500)
- *7) PA6,6 viscosity number: 120 ml/g; $[\text{NH}_2] = 2.5 \times 10^5 \text{ mol/g}$; $[\text{COOH}] = 11.6 \times 10^5 \text{ mol/g}$
- *8) PA6,6 viscosity number: 130 ml/g; $[\text{NH}_2] = 4.2 \times 10^5 \text{ mol/g}$; $[\text{COOH}] = 9.1 \times 10^5 \text{ mol/g}$
- *9) PA6,6 viscosity number: 230 ml/g; $[\text{NH}_2] = 2.4 \times 10^5 \text{ mol/g}$; $[\text{COOH}] = 4.8 \times 10^5 \text{ mol/g}$
- *10) PA6,6/6,I containing 19 mol% of polyamide 6I; $[\text{NH}_2] = 3.9 \times 10^5 \text{ mol/g}$; $[\text{COOH}] = 10.2 \times 10^5 \text{ mol/g}$

(11) Please amend the Table 2 at page 94 as follows:

Table 2

		Ex. 5	Comp. Ex. 2	Ex. 6	Ex. 7
Upstream inlet					
Feeder 1	PPE-1 (parts by weight)	38	38	38	22
Feeder 2	MPPE (parts by weight)				16
	MAH (parts by weight)	0.3	0.3	0.3	
Feeder 3	SEBS1 (parts by weight)	12		12	3
	SEBS2 (parts by weight)		12		5
	SEBS3 (parts by weight)	*11			4
1st downstream inlet					
Feeder 4	PA66-a (parts by weight)			50	20
	PA66-b (parts by weight)	30	30		10
	PA66-c (parts by weight)				
	PA-MB (parts by weight)	*12	20	20	20
	KB (parts by weight)	*13		2	
Polyamide area ratio		%	81	75	96
PPE having a molecular weight of 5,000 or less		%	-	-	3.12
PPE having a molecular weight of 200,000 or less		%	-	-	0.92
PPE having a molecular weight of 200,000 or less/ PPE having a molecular weight of 50,000 <u>5,000</u> or less		-	-	-	0.29
Coating adhesion strength (number of square coating sections left on the surface of a shaped resin article out of 100 square coating sections)			83	45	70
Sharpness of an image reflected in the coated surface		-	B	A	B

Matteness of the coated surface

IV

IV

II

III

-

- *11) SEBS block copolymer (styrene content: 60 %; Mn: 105,000)
- *12) Conductive polyamide/carbon masterbatch (carbon content: 10 wt%)
- *13) Conductive carbon (keijon black EC600JD)